Characterization of Micropore Structure of Porous Materials Using DFT Models Applied to Ar, N₂ and H₂ Adsorption Data.

> Jacek Jagiello Micromeritics Instrument Coorporation, Norcross GA, USA

> > jacek.jagiello@miromeritics.com



Outline of the presentation

- Objective
- Earlier results
- Experimental
- Assumptions of model calculations
- Method of the PSD calculation
- Calculation of carbon PSDs using multiple adsorbates: Examples
- Fundamental and practical advantages of using more than one adsorbate for PSD analysis
- DFT based prediction of high-pressure H_2 adsorption at ambient temperature from H_2 measurements at 77 K
- PSD analysis for zeolites
 - Effect of pore sizes and materials chemistry
- Conclusions



Objective

Discussion of the micropore structure analysis of porous {nanoporous, microporous} materials based on adsorption measurements of standard adsorbates N₂ and Ar, and H₂ isotherms

at cryogenic temperatures.



Earlier results Comparison of PSDs calculated from different adsorbates









J. Jagiello, M. Thommes, Carbon Conference, Oviedo (2003) Carbon 42,1227–1232 (2004)



Earlier results H₂ Adsorption on Takeda 3A Carbon Molecular Sieve



Figure 1. Experimental H₂ isotherm measured at 87 K for the Takeda 3A sample compared with the NLDFT isotherms calculated for the 3 and 4 Å pores and with the curve fitted by SAIEUS.

Jagiello, J.; Thommes M.; Linares-Solano, A.; Cazorla-Amorós, D.; Lozano-Castelló, D., Extended Abstracts, Carbon 2004



Experimental

Materials

Set 1:

Carbons derived from poly(ethylene terephthalate), PET Sample PC obtained by pyrolysis of PET.

Samples PC12, PC35, PC58, and PC76 obtained from PC by CO₂ activation with increasing burn-off (12, 35, 58, 76 %)

Details: Parra JB, Ania CO, Arenillas A, Rubiera F, Palacios JM, Pis JJ., J Alloys Compd, 379: 280–89 (2004)

Set 2:

Commercial CMSs from Supelco obtained from polymeric precursors Details: Jagiello, J., Betz, W. Microporous and Mesoporous Materials, **108**, 117–122 (2008)

Sample ACF10, Activated carbon fiber (Kynol)

Details: Jagiello, J., Thommes, M. Carbon 42,1227–1232 (2004)

Commercial Zeolite Samples (Aldrich)



Outline of model calculations

- Model **NLDFT** isotherms (kernels) are calculated using **Tarazona** approach [1, 2].
- Slit pore model for carbon pores.
- Carbon-gas interactions described by the **Steele potential** [3].
- LJ parameters for N_2 and Ar taken from **Ravikovitch** et al. [4].
- Weeks-Chandler-Andersen attractive potential [2].
- H_2 - H_2 interactions: **Silvera-Goldman** [5] potential modeled by LJ potential [6] $e_{\rm ff}/k = 34.3$ K, $s_{\rm ff} = 3.04$ Å
- Gas-solid interaction parameters for H₂-carbon derived from the fit to experimental isotherm measured on graphitized carbon black [7]
- Quantum corrections for H₂ model applied by using **Feynman** "Effective Potential."
- The cylindrical pore model is assumed for zeolite pores.
- 1. Tarazona P, Marini Bettolo Marconi U, Evans R. Mol Phys 1987;60:573.
- 2. Lastoskie C, Gubbins KE, Quirke N. J Phys Chem 1993;97:4786-96.
- 3. Steele WA. The Interactions of Gases with Solid Surfaces Pergamon, Oxford, 1974.
- 4. Ravikovitch PI, Vishnyakov A, Russo R, Neimark AV. Langmuir 2000;16:2311-2320.
- 5. Silvera IF, Goldman VV. J Chem Phys 1978; 69: 4209
- 6. Stan G, Cole MW. J. Low Temp. Phys. 1998; 110:539-544.
- 7. J. Jagiello, A. Anson, M.T. Martinez, J. Phys. Chem., 110 (2006) 4531



Outline of the PSD calculation method

Multi Adsorbate Integral Equation [1]:

$$\min\sum_{m}\sum_{i}^{M}\sum_{i}^{N_{m}} \left[V_{m}(p_{i}) - \int_{\alpha_{m}}^{\beta_{m}} K_{m}(p_{i}, w) f(w) dw \right]^{2}$$
(1)

p_i - experimental pressure of i-th adsorption point

 V_m - measured adsorption isotherm for m-th adsorbate

K_m- set of theoretical DFT isotherms (Kernel) for m-th adsorbate model

f(w) - PSD

w - effective pore width

M - number of adsorbates/models

N_m - number of points of m-th experimental isotherm

f(w) is obtained by conditional minimization of (1) using regularization, SAIEUS [2], nonnegativity constraints [3], L-curve [4].

[1] Jagiello, J.; Thommes M.; Linares-Solano, A.; Cazorla-Amorós, D.; Lozano-Castelló, D., Extended Abstract, Carbon 2004

[2] Jagiello, J. Langmuir 1994, 10, 2778

[3] Lawson, C. L.; Hanson, R. J. Solving Least Squares Problems; Prentice-Hall: Englewood Cliffs, New Jersey, 1974

[4] Hansen, P. C.; O'Leary, D. P. SIAM J. Sci. Comput. 1993, 14, 1487





J. T. Duda, L. Jagiello, J. Jagiello, J. Milewska-Duda, Appl. Surface Sci., 253, 5616–5621 (2007)





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Using Isotherms at Sub and Super Critical Temperatures



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Analysis of adsorption isotherms for series of PC carbons



Multi versus single adsorbate fit

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Calculated PSDs for PC samples

Differential

Cumulative



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Fitting Ar and H₂ isotherms measured on CMS samples



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Calculated PSDs for CMS samples

Differential

Cumulative



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Effect of using truncated Ar data (Carboxen-1021)



Calculated PSD

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Prediction of High-Pressure H₂ Adsorption

Standard Adsorption Properties Derived from Ar Isotherms (87 K)



Sample	S(BET) m²/g	V _m (DR) cm³/g
Maxsorb	2100	0.69
Carbosieve	1120	0.42
Norit	970	0.37

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Micro pore Analysis Using H₂ Adsorption



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Prediction of H₂ Adsorption at 87 and 298 K from Adsorption Isotherms at 77 K Based on DFT Model



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Effects of pore size and chemistry in analysis of zeolite pore structure

Cylindrical pore model is assumed for zeolite pores.

Model NLDFT isotherms (kernels) are calculated using Tarazona approach.

Fluid-pore interaction potential has the following form:

 $U_{pore} = E_{wall}(\rho, \varepsilon_{sf}) U_{cylinder}(w, r)$

where:

 $\label{eq:result} \begin{array}{l} \rho \mbox{ - the solid density} \\ \epsilon_{sf} \mbox{ - the adsorbate-solid atom interaction parameter} \\ w \mbox{ - the effective pore width} \\ r \mbox{ - the distance of a molecule from the pore wall} \\ E_{wall} \mbox{ - the wall potential interaction parameter} \\ U_{cvlinder} \mbox{ - the fluid-cylindrical wall interaction potential} \end{array}$



Effects of pore size and chemistry on gas adsorption in zeolites

N₂ Adsorption Isotherm Measured for Zeolite Y Sample



PSDs clculated for Y-N₂ data using

different E_{wall} parameters





Analysis of N₂ and Ar Adsorption Isotherms for Zeolite X and Y Samples

Adsorption Isotherms for Zeolite X



Adsorption Isotherms for Zeolite Y



PSDs Calculated using Optimal E_{wall} parameters





Analysis of N₂ and Ar Adsorption Isotherms for ZSM5 Sample (NH₄ form)





PSD Peak Position as a Function of Wall Potential Parameter, E_{wall}

Ar

 N_2



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Conclusions

- Carbon PSDs obtained from the simultaneous analysis of multiple adsorption isotherms are robust and consistent with more than one adsorbate.
- This approach allows detecting experimental points that are not fully equilibrated due to very slow diffusion to narrow micropores.
- The range of pore size analysis is extended to smaller pore sizes compared to the standard nitrogen or argon adsorption analysis.
- Data of the two isotherms provide complementary information about the carbon porosity in the range of micro and mesopores.
- Proposed approach can be considered a useful tool for a comprehensive characterization of activated carbons, and for obtaining detailed and reliable carbon PSDs.
- Effective pore wall potential assumed for zeolites allows separating geometrical and chemical effects in the analysis of zeolite pore structure.



PSDs calculated for Y-N2 data using different Ewall parameters.

N2 and Ar Adsorption Isotherms for Zeolite X Sample PSDs calculated for Y and X data using Ewall parameters from Table 1

N₂ and Ar Adsorption Isotherms for Zeolite Y Sample

N2 and Ar Adsorption Isotherms for ZSM5 Sample

PSDs clculated for ZSM5 data using Ewall parameters from Table 1

